

General Physics I

Lect.21 State Variables



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Variables in thermodynamics

- The subject of thermodynamics is complicated because there are so many different ways of describing the same thing.
- For a gas, ideal gas law PV=NkT, we can say pressure depends on the temperature and on the volume P(V,T), or volume depends on the temperature and the pressure V(T,P). For *internal energy* U, we can have U(T,V), or U(T,P), or U(P,V). For *entropy*, S(T,V). And we can construct many other variables as we like, such as: U–TS.
- For simplicity, we consider variables **T** and **V**, and their dependent functions **U** and the **P**. Everything else should be a function of them.
- Since the variable of P depend on V and T, <u>ordinary derivative</u> dP/dT is not enough. We define a new math symbol called <u>partial derivative</u>, ∂P/∂T. This remind us that P depends on V, as well as on T. To show that the other variable is held constant, we write the variable that is held constant as a subscript, (∂P/∂T)_V

Partial differentials

If a function rely on multiple variables, e.g., f(x,y), its partial differentials follows:

$$\left(rac{\partial f}{\partial x}
ight)_y = \liminf_{\Delta x o 0} rac{f(x+\Delta x,y)-f(x,y)}{\Delta x}$$

$$\left(rac{\partial f}{\partial y}
ight)_x = \liminf_{\Delta y o 0} rac{f(x,y+\Delta y)-f(x,y)}{\Delta y}.$$

 $\partial^2 f / \partial x \partial y = \partial^2 f / \partial y \partial x$ (commutation)







$$f: \mathbb{R}^3 \to \mathbb{R}, \vec{v}: \mathbb{R}^3 \to \mathbb{R}^3$$

$$\begin{array}{l} \text{Gradient: } \nabla f \equiv \left(\frac{\partial f}{\partial x_1}, \frac{\partial f}{\partial x_2}, \frac{\partial f}{\partial x_3}\right) \\ \text{Divergence: } \nabla \cdot \vec{v} \equiv \frac{\partial v_1}{\partial x_1} + \frac{\partial v_2}{\partial x_2} + \frac{\partial v_3}{\partial x_3} \\ \text{Curl: } \nabla \times \vec{v} \equiv \left(\frac{\partial v_3}{\partial x_2} - \frac{\partial v_2}{\partial x_3}, \frac{\partial v_1}{\partial x_3} - \frac{\partial v_3}{\partial x_1}, \frac{\partial v_2}{\partial x_1} - \frac{\partial v_1}{\partial x_2}\right) \\ \text{Laplacian: } \nabla^2 f \equiv \frac{\partial^2 f}{\partial x_1^2} + \frac{\partial^2 f}{\partial x_2^2} + \frac{\partial^2 f}{\partial x_3^2} \end{array}$$



Specific heat at constant volume

When the temperature changes from T to T+ Δ T and the volume changes from V to V+ Δ V, change in the internal energy U(T,V) is:

$$\Delta U = \Delta T igg(rac{\partial U}{\partial T} igg)_V + \Delta V igg(rac{\partial U}{\partial V} igg)_T$$

From the first law we have:

$$\Delta U = \Delta Q - P \, \Delta V$$
 .

Let's first keep the volume constant $(\Delta V=0)$ to derive the heat capacity. With $\Delta Q=\Delta U=0$, and from above that $\Delta U=\Delta T(\partial U/\partial T)_V$, so we have $(\partial U/\partial T)_V=\Delta Q/\Delta T$. This value means the amount of heat one needs to increase unit temperature of a substance, called the *specific heat at constant volume* (C_V).

$$\left(rac{\partial U}{\partial T}
ight)_V = C_V$$

Fundamental relations in thermodynamics

Consider a Carnot cycle, the total amount of work done by the gas in a reversible cycle is $\Delta Q(\Delta T/T)$, where ΔQ is the amount of heat energy added. From *geometry* of right bottom plot, we know that from

$$\Delta V \Delta P = \Delta Q \left(rac{\Delta T}{T}
ight)$$

 $rac{\Delta T}{T} \cdot \begin{pmatrix} \text{heat needed} \\ ext{to change } V \\ ext{by } \Delta V \end{pmatrix}_{ ext{constant } T} = \Delta V \cdot \begin{pmatrix} ext{change in } P \\ ext{when } T \text{ changes} \\ ext{by } \Delta T \end{pmatrix}_{ ext{constant } V}$

The heat needed to expand: $\Delta Q = T \left(\frac{\partial P}{\partial T} \right)_V \Delta V$

 ΔU can be written as the sum of ΔQ and the work done: $\Delta U = T \left(\frac{\partial P}{\partial T}\right)_V \Delta V - P \Delta V$.

Now we find the rate of change of U with V at constant T:

$$\left(rac{\partial U}{\partial V}
ight)_T = T \left(rac{\partial P}{\partial T}
ight)_V - P$$

 $-\Lambda V$ PRESSURE $T - \Delta T$ VOLUME ΔV P ΔP P-V diagrams for a Carnot cycle

Only P, V, U, T appear in this fundamental equation, and can be used to deduce other thermodynamic results.



Ideal gas at constant temperature

Assume we have an ideal gas at constant temperature T, so $\Delta U=0$ as U only depend on T. So we have $\left(\frac{\partial U}{\partial U}\right)_{-} = T\left(\frac{\partial P}{\partial U}\right)_{-} - P = 0$

$$\left(\frac{\partial U}{\partial V}\right)_T = T\left(\frac{\partial P}{\partial T}\right)_V - P = 0$$

From integration (we write out "const V" as a reminder) we have

 $\ln P = \ln T + {
m const}; \quad {
m const} \ V,$

 $P = \mathrm{const} imes T; \qquad \mathrm{const} \ V.$

This agrees with the ideal gas law that PV=NkT. Recall that at one stage we assumed that the kinetic energy of the molecules was proportional to the temperature, which we call it the **ideal gas scale**, or **kinetic temperature**.

Here from the Second Law we defined we define the **grand thermodynamic absolute temperature**, which based on the Carnot cycles it is completely independent of the working substance, but rather the fundamental rule of thermodynamic.

It's nice to have the two temperature scales unified!

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Enthalpy

Recall that $\Delta U = \Delta Q - P \Delta V$; we can play a trick to replace P ΔV with V ΔP . Let's define a new state variable called **enthalpy (焓)**, its dictionary definition is the total heat content of a system, most used by chemists. Observe that d(PV)=PdV+VdT:

 $egin{aligned} \Delta(PV) &= P\,\Delta V + V\,\Delta P \ \Delta U &= \Delta Q &- P\,\Delta V \ \hline \Delta(U+PV) &= \Delta Q &+ V\,\Delta P \end{aligned}$

So now we have $\Delta H = \Delta Q + V \Delta P$, compared with ΔU , we have the following rules: $U \rightarrow H, P \rightarrow -V, V \rightarrow P$. The fundamental relationship becomes

$$\left(rac{\partial H}{\partial P}
ight)_T = -T \left(rac{\partial V}{\partial T}
ight)_P + V.$$

Similarly, we can show that the heat capacity at constant pressure is

$$\left(\frac{\partial H}{\partial T}\right)_{p} = C_{p}$$

Helmholtz free energy



Helmholtz Free Energy is a thermodynamic potential that measures the "useful" work obtainable from a closed thermodynamic system at a constant temperature and volume. The derivation is very similar to the last slide, where d(TS)=TdS+SdT, s.t.

dU=d(TS)-SdT-PdV

d(U-TS)=-SdT-PdV

We define a new variable F=U-TS and have the relation of dF=-SdT-PdV. From that, compared with dU=TdS-PdV, we can use the rules $U\rightarrow F$, $S\rightarrow T$, $T\rightarrow -S$ to derive the fundamental relationship involving F.

One can find expressions for entropy and pressure:

$$\left. S = - \left(rac{\partial F}{\partial T}
ight)
ight|_V \qquad P = - \left(rac{\partial F}{\partial V}
ight)
ight|_T$$

Clausius-Clapeyron equation

*Previously, we derived work done = ΔQ

- Consider some liquid (so not ideal gas) in a cylinder, if we keep the temperature constant, we have an isothermal line on the P-V diagram which involve the phase change between liquid and gas.
- Now connect the two isothermal lines with adiabatic lines, the heat ٠ added to the substance in changing it from a liquid to a vapor is related to the work done by the substance as it goes around the cycle.
- Such heat is usually called the **Latent heat**, denoted by **L**. Using ٠ the analogy of the previous Carnot's argument*, we can now equate $L(\Delta T/T)$ and $\Delta P(V_G - V_I)$ [see bottom plot]. Similarly to previous example, we write

$$rac{L}{T(V_G-V_L)}=(\partial P_{
m vap}/\partial T)$$

For each mole, $V_G = V_L \approx V_G = RT/P$, and hence $\partial P/\partial T = L/(RT^2/P)$. So • the solution is in the form of $P = const e^{-L/RT}$, which is very similar to the results from the result derived from kinematic theory

$$n = \left(\frac{1}{V_a}\right) e^{-(U_G - U_L)/RT} \longrightarrow P = nkT = \left(\frac{kT}{V_a}\right) e^{-(U_G - U_L)/RT}$$
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Clausius-Clapeyron equation (cont)



Rather, U_G - U_L is constant, independent of temperature, then the two **P-T** relations are equal. Since the pressure is constant while the volume is changing, the change in internal energy U_G - U_L is equal to the heat L put in minus the work done $P(V_G$ - $V_L)$, so $L=(U_G+PV_G)-(U_L+PV_L)$ or $L=H_G$ - $H_L=\Delta H$.

- 1. In the phase change, the enthalpy plays the role of internal energy.
- 2. Unlike ideal gas energy states is purely a state of temperature, states of evaporation also depends on the pressure (see xenon).
- 3. From thermodynamic relation, this the argument is true for any other change of state, i.e., solid-to-liquid: $(\partial P_{melt}/\partial T)_V = M/[T(V_{liq}-V_{solid})]$



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Heat capacities, latent heats, Gibbs energy (in terms of entropy)

• For reversible process, we can express heat capacities in terms of entropy:

$$C_V = (\frac{dQ}{dT})_V = T(\frac{dS}{dT})_V$$
 and likewise, $C_P = T(\frac{dS}{dT})_P$

- For latent heat (heat needed to convert unit mole from one phase to another) the expression is $L = \Delta Q = T\Delta S$. We can see that the heat exchange in the phase change comes from the change of entropy, even T and P can stay at constant.
- Now equate $L=(U_G+PV_G)-(U_L+PV_L)$ and is $L=T(S_G-S_L)$ and rearrange, and define a new expression called Gibbs free energy*, G=H-TS:

 $G_G = (U_G + PV_G) - TS_G = U_L + PV_L - TS_L = G_L$

*depends on T and P

		Heat of Vap.	ΔS of Vap.
	Bpt/K	(kJ/mol)	(J/K/mole)
H ₂	20	0.46	23
Ne	27	1.7	63
Butane	273	21	77
NH ₃	240	23	97
H ₂ 0	373	41	109
AI	2792	294	105
Fe	3134	340	108

Latent heat and entropy change for changes in different substances.

Gibbs free energy is, again, a thermodynamic state variable to predict spontaneous chemical reactions (ΔG <0).

Entropy for ideal gas

• For ideal gas, assuming constant number of molecules, we have, and we define a new quantity, heat capacity per mole, $C_{V,m}=C_V/n$, s.t.

 $dU=TdS-PdV=nC_{V,m}dT$ $dS=(dU+PdV)/T = (nC_{V,m}dT+PdV)/T$ $= (nC_{V,m}dT+nRTdV/V)/T$

 $= n(C_{V,m}dT/T+RdV/V)$

S=nC_{V,m}lnT+nRln(V/n)+const.

- The constant term we cannot directly derive from thermodynamical analysis (though we can probably guess it's proportional to n).
- Setting S=0, we have the adiabatic process, so $C_{V,m}lnT_1+RlnV_1=C_{V,m}lnT_2+RlnV_2$
- We can show that $T_1V_1^{\gamma-1} = T_2V_2^{\gamma-1}$

Back to the example in the last lecture, the expansion of gas into vacuum: $\Delta U = \Delta Q = \Delta W = 0$ pVT p' V' T' remove partitio $\Delta U = 0$, $\Delta T = 0$ for an ideal gas T = T'. Per mole of gas we have $\Delta S = C_V \ln(T/T') + R \ln(V/V')$ = Rln(V/V') > 0 for V'>V



Summary of state variables

	$\left(\partial F \right) \right $
$\mu = $	$\left(\left.\overline{\partial N}\right)\right _{T,V}$

Name	Symbol	Formula	Natural variables
Internal energy	U	$\int (TdS - pdV) + \sum_{i} \mu_{i} dN_{i}$	$S, V, \{N_i\}$
Hemholtz free energy	F	U - TS	$T, V, \{N_i\}$
Enthalpy	Н	U + pV	$S, p, \{N_i\}$
Gibbs free energy	G	U + pV - TS	$T, p, \{N_i\}$